

Thermosolutal natural convective transport in Casson fluid flow in star corrugated cavity with Inclined magnetic field

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ABSTRACT

Diffusion mechanism generated because of thermal and solutal buoyant forces in star corrugated cavity filled with Casson liquid is envisioned in this study. Magnetic field making angle of inclination with enclosure is also taken into account. Rectangular plate with isothermal and isoconcentration distributions is installed. To measure optimized variation in associated distributions all the extremities of enclosure are kept at cold temperature and zero concentration. Governing equations are modelled by incorporating conservation laws. After then, complexly formulated model equations and their associated boundary constraint are change in dimensionless structure by obliging variables. Numerical simulations are performed by opting finite element based commercial software renowned as COMSOL. Domain is discretized in the form of triangular and rectangular elements by executing hybrid meshing. Afterwards, non-linear solver (PARADISO) is capitalized to handle system of non-linear equations. Mesh independence test is carried out to assure credibility of conducted simulations. Comparison of results with published literature is also displayed. Graphical and tabular representation describing change is associated fields (velocity, temperature and concentration) against wide range of involved parameters. Change in kinetic energy along with average Sherwood and Nusselt number against different magnitudes of Casson parameter is divulged through tables.

Introduction

Diffusion transport mechanism in liquids resulting due to thermal and species concentration changes is denoted as thermosolutal convection. Depending on orientation of gradients existed during the flow in enclosures multiple type of diffusions occurs. Among these thermosolutal convection has received promising applications in diversified fields, e.g. thermal engineering, geophysics and astrophysics. In addition, in geothermal phenomena the role of stratification produced due to variation in intensification of temperature and solutal distributions is highly beneficial in crystal growth, oceanography and management of water reservoirs. Some highly recommendable utilizations related to current topic are encapsulated in [1–11]. Beghein et al. [12] carried out analysis on effectiveness of assisting and opposing solutal buoyancy force on steady state thermosolutal convection in air enclosed in square

cavity. Numerical simulations were performed by Gobin and Bennacer [13] to contemplate multicellular flow structure of binary fluid contained in an enclosure with imposition of horizontal thermosolutal differences. Examination about diffusion under joint influence of inertial and thermal/solutal buoyancy forces was divulged by Aimiri et al. [14]. Deposition of nanocomposite on electrodes by varying mass diffusivities with static magnetization was delineated by Zhou et al. [15]. A comprehensive analysis on effect of variation in aspect ratio of annular region on heat mass transport in domain was visualized by Chen et al. [16]. Kefayati and his coauthors [1,17–19] performed computational simulations by LBM method to explicate thermal and solutal diffusivity phenomenon in closed domains with numerous physical aspects. In addition, for the sake of interest of readers and keeping essence of work in mind some related work is provided in refs. [11,20–25].

Materials possessing elastic characteristics and requires specific

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threshold of stress for producing deformation is recognized as viscoelastic liquids. The effectiveness and appliance of these materials are observed in daily life products e.g. Combination of paints with polymers and solver is good use of these materials and obliged in buildings for renovations along with fabrication of complexed surfaces. Other than this viscoelastic materials also characterizes the features of blood and efficiently used in DNA replication process. Packaging of drugs and refinement of curde oil are also the examples which describes employment of these materials. For comprehensive response of viscoelastic materials against yielding stress at high shearing viscosity formulating mathematical framework was demarcated by Casson [26]. After this an extensive work on Casson fluid with multiple physical aspects are discussed like Rao et al. [27] delineated impact of surface drag force on yielding stress and found that for infinite shear stress at surface the fluid will behave as solid. Bird et al. [28] analyzed rheology of materials with yields by utilizing Casson fluid model and measured driving gradients beyond and below the critical stress. Some research studies describing the importance and characteristics of viscoelastic materials by incorporating Casson model is disclosed in refs. [29–33].

Transportation of fluid regimes under the implementation of transverse magnetization make them more potentially more applicable in different governing problems rather in absence. The liquids which polarizes and respond to magnetic field are called as electrically conducting. In addition, these magnetized liquids store extra energy due to polarization and thus employed in numerous engineering systems like reactor frameworking, coolant in reactors, packaging of instruments, growths of crystals, solar panels and so forth. Garandet et al. [34] demonstrated stratified flow of water in rectangular cavity generated by magnetization and buoyant forces. Rudrariah et al. [35] found decrement in momentum and thermal diffusivities of liquid by providing magnetization. Scaling procedure was opted by Hadid et al. [36] to defined dimensionless representation of magnetic strength parameter for description of flow in different physical circumstances. Tagawa and Ozoe [37] delineated convective flow of mettalic liquid in a cube by applying static magnetic field and measure depreciation in momentum and enhancement in thermal field against Hartmann number. Problem formulation for single phase nanofluid flow in wavy cavity for wide range of Hartmann number was adumbrated by Sheremet et al. [38]. Kifayati and his coresearchers [39,40] comprehended changes in convective flow of liquids in different shaped cavities by executing uniformly palced magnetic source. Latest developments on convective flow of ordinary and nanofluid flow in confined geometries by measuring diffusion with physical prospectives of magnetic field and instalment of objects are encapsulated in [41–48].

It is prompted from accessible literature review and analyzing extensive appearance of thermally and solutaly convective diffusion transport in diversifed processes this effort is made. Subsequently, so far examination of above said physical features are not interrogated even with viscous liquid. But in this document we have performed advance study by obliging Casson liquid in star enclosure with corrugations and with employment of magnetic field with inclination. So, the prime consent of all author is on to fill this breach. For this purpose a rectangular fin is installed by providing constant heat and mass distributions. Additionally, results are validated by constructing limitized situation for present case study and compared with existed results.

Formulation of problem

Description statement

A star shaped enclosure with corrugation filled with laminar and incompressible flow of Casson liquid is taken into account. A rectangular fin of unit length by providing constant temperature and concentration distribution is also installed. Fluid density is assumed to be the function temperature and concentration gradients due to which convection in domain is generated. Inclining magnetic field of uniform strength

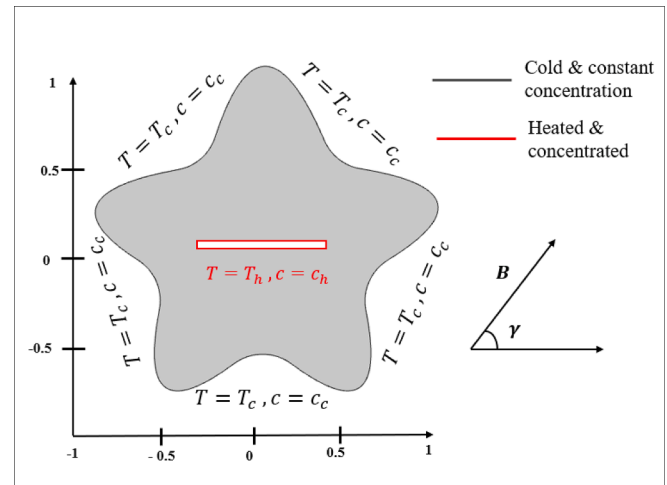


Fig. 1. Graphical description of domain.

forming angle γ is considered. Graphical visualization of domain is displayed in Fig. 1.

Constitutive equations

A Casson fluid model constitutive equation describing the connection between stress and deformation rate is mentioned below [48].

$$\sqrt{\tau^*} = \sqrt{\mu \dot{\gamma}^*} + \sqrt{\tau_0^*}, \text{ for } \tau^* \geq \tau_0^*,$$

$$\dot{\gamma}^* = 0, \text{ for } \tau^* \leq \tau_0^* \quad (1)$$

here, τ^* and τ_0^* represent shearing and yielding stresses.

The governing transport equations for considered problem is as follows [36].

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (2)$$

$$\rho \left(u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right) = -\frac{\partial p}{\partial x} + \mu \left(1 + \frac{1}{\beta} \right) \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) + \Lambda_x \quad (3)$$

$$\rho \left(u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right) = -\frac{\partial p}{\partial y} + \mu \left(1 + \frac{1}{\beta} \right) \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) + \Lambda_y \quad (4)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha_c \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) \quad (5)$$

$$u \frac{\partial c}{\partial x} + v \frac{\partial c}{\partial y} = D \left(\frac{\partial^2 c}{\partial x^2} + \frac{\partial^2 c}{\partial y^2} \right) \quad (6)$$

Here, Λ denotes the forcing factor generated due to magnetization.

After utilizing Boussinesq approximation the forcing factor takes following form.

$$\Lambda_x = \sigma B_0^2 (v \sin \gamma \cos \gamma - u \sin^2 \gamma) \quad (7)$$

$$\Lambda_y = \sigma B_0^2 (u \sin \gamma \cos \gamma - v \cos^2 \gamma) + \rho g [\beta_T (T - T_c) + \beta_c (c - c_c)] \quad (8)$$

Where, β_T and β_c shows the thermosolutal diffusivities, respectively.

Prescribed wall conditions

$$u = 0, v = 0, T = T_h, c = c_h, \left(-\frac{L}{2} \leq x \leq \frac{L}{2} \right), y = 0 \quad (9)$$

$$u = 0, v = 0, T = T_c, c = c_c, -L \leq x \leq L, -L \leq y \leq L \quad (10)$$

Utilization of below mentioned set of variable for conversion into dimensionless representation.

$$(X^*, Y^*) = \frac{(x, y)}{L}, (U^*, V^*) = \frac{(u, v)L}{\alpha}, P^* = \frac{pL^2}{\rho\alpha^2}, \theta^* = \frac{T - T_c}{T_h - T_c}, C^* = \frac{c - c_c}{c_h - c_c} \quad (11)$$

$$\alpha_e = \frac{k_e}{(\rho c_p)_f}, Ra = \frac{\rho^2 \beta_T g L^3 \Delta T Pr}{\nu^2}, Le = \frac{\alpha_e}{D}, Ha = BL \sqrt{\frac{\mu}{\sigma}}, Pr = \frac{\nu}{\alpha} \quad (12)$$

Non-dimensional visualization of transport equations is attained below [48].

$$\frac{\partial U^*}{\partial X^*} + \frac{\partial V^*}{\partial Y^*} = 0 \quad (13)$$

$$\left(U^* \frac{\partial U^*}{\partial X^*} + V^* \frac{\partial U^*}{\partial Y^*} \right) = -\frac{\partial P^*}{\partial X^*} + Pr \left(1 + \frac{1}{\beta^*} \right) \left(\frac{\partial U^*}{\partial X^*} + \frac{\partial U^*}{\partial Y^*} \right) + \Lambda_{X^*} \quad (14)$$

$$\left(U^* \frac{\partial V^*}{\partial X^*} + V^* \frac{\partial V^*}{\partial Y^*} \right) = -\frac{\partial P^*}{\partial Y^*} + Pr \left(1 + \frac{1}{\beta^*} \right) \left(\frac{\partial V^*}{\partial X^*} + \frac{\partial V^*}{\partial Y^*} \right) + \Lambda_{Y^*} \quad (15)$$

$$U^* \frac{\partial \theta^*}{\partial X^*} + V^* \frac{\partial \theta^*}{\partial Y^*} = \frac{\partial^2 \theta^*}{\partial X^{*2}} + \frac{\partial^2 \theta^*}{\partial Y^{*2}} \quad (16)$$

$$U^* \frac{\partial C^*}{\partial X^*} + V^* \frac{\partial C^*}{\partial Y^*} = \frac{1}{Le} \left(\frac{\partial^2 C^*}{\partial X^{*2}} + \frac{\partial^2 C^*}{\partial Y^{*2}} \right) \quad (17)$$

Where,

$$\Lambda_{X^*} = Pr Ha^2 (V^* \sin \gamma \cos \gamma - U^* \sin^2 \gamma) \quad (18)$$

$$\Lambda_{Y^*} = Pr Ha^2 (U^* \sin \gamma \cos \gamma - V^* \cos^2 \gamma) + Ra Pr (\theta^* + NC^*). \quad (19)$$

Conditions at boundaries of domain in dimensionless structuring is as under.

$$U^* = 0, V^* = 0, \theta^* = 1, C^* = 1 \left(-\frac{1}{2} \leq X^* \leq \frac{1}{2}, Y^* = 0 \right) \quad (20)$$

$$U^* = 0, V^* = 0, \theta^* = 0, C^* = 0 \left(-1 \leq X^* \leq 1, -1 \leq Y^* \leq 1 \right) \quad (21)$$

Correlations defining local and mean heat and mass fluxes are described below.

$$Nu_{local} = -\frac{\partial \theta^*}{\partial n} \bigg|_{innerwall}, \quad (22)$$

$$Sh_{local} = -\frac{\partial C^*}{\partial n} \bigg|_{innerwall}, \quad (23)$$

$$Nu_{avg} = \frac{1}{L} \int_L Nu_{local} dL, \quad (24)$$

$$Sh_{avg} = \frac{1}{L} \int_L Sh_{local} dL. \quad (25)$$

Additionally, globally quantified kinetic energy is shown as under.

$$K.E = \frac{1}{2} \int_{\Omega} \|U\|^2 d\Omega. \quad (26)$$

Computational scheme

Transport mechanism in fluids in simple confined geometries is easily managed by exact approaches and traditional schemes. But, most of the problems in nature arises is intricate structural designs so previously implemented exact schemes are unable to solve them. For this

Table 1

Meshing at different level of refinements.

Grid	# EL	#DOFs
Extremely coarse	390	2607
Extra coarse	552	3630
Coarser	878	5643
Coarse	1476	9284
Normal	2130	13,189
Fine	3388	20,504
Finer	8092	48,224
Extra fine	20,002	117,161
Extremely fine	27,678	159,379

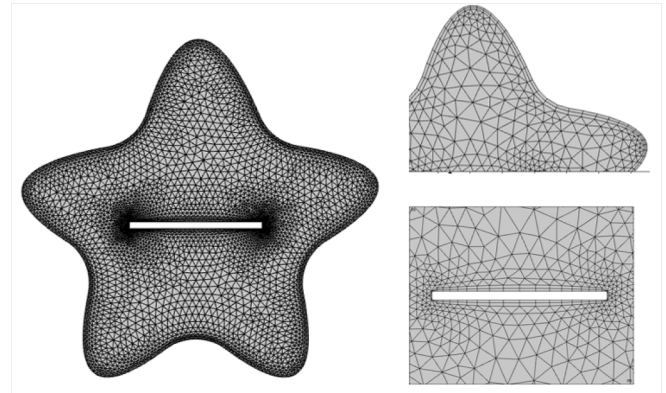


Fig. 2. Element formation in domain at coarser grid.

propose the analytical approaches are found to be the best for solving these problems. Specifically discussing about the irregular shapes the flow phenomenon is efficiently tackled by versatile method known as finite element method. In this procedure the domain is divided into small portions and variable of interest are computed at element level. Depending on field variables degrees of freedom are computed at different refinement levels as shown in Table 1 and interpolated by utilizing stable element pair. Since, the governing problem discussed here comprises of pressure which is approximated by linear polynomials where as rest of distributions are approximated by quadratic polynomials. Discretization of domain is manifested in Fig. 2 describing hybrid meshing at coarse level with triangular and rectangular elements. Afterwards, system of non-linearized equations are formed and solved by direct solver known as PARADISO. The steps involved in the scheme are presented in Table 1. Convergence criterion adjusted for nonlinear iterations is as follows

$$\left| \frac{\chi^{n+1} - \chi^n}{\chi^{n+1}} \right| < 10^{-6}$$

Where, χ characterizes the general solution component (Fig. 3).

Discretization of equations (Weak Formulation)

Let subspace for U^*, V^*, θ^*, C^* is $W = [H^1(\Omega)]^3$ be the test subspaces for pressure is $Q = L^2(\Omega)$. The weak form of the governing equation is given as.

$$\begin{aligned} \int_{\Omega} \left(U^* \frac{\partial U^*}{\partial X^*} + V^* \frac{\partial U^*}{\partial Y^*} \right) w d\Omega + \int_{\Omega} \frac{\partial P^*}{\partial X^*} w d\Omega + Pr \int_{\Omega} \left[\left(1 + \frac{1}{\beta^*} \right) \left(\frac{\partial U^*}{\partial X^*} + \frac{\partial U^*}{\partial Y^*} \right) + \Lambda_{X^*} \right] w d\Omega \\ = 0, \end{aligned} \quad (27)$$

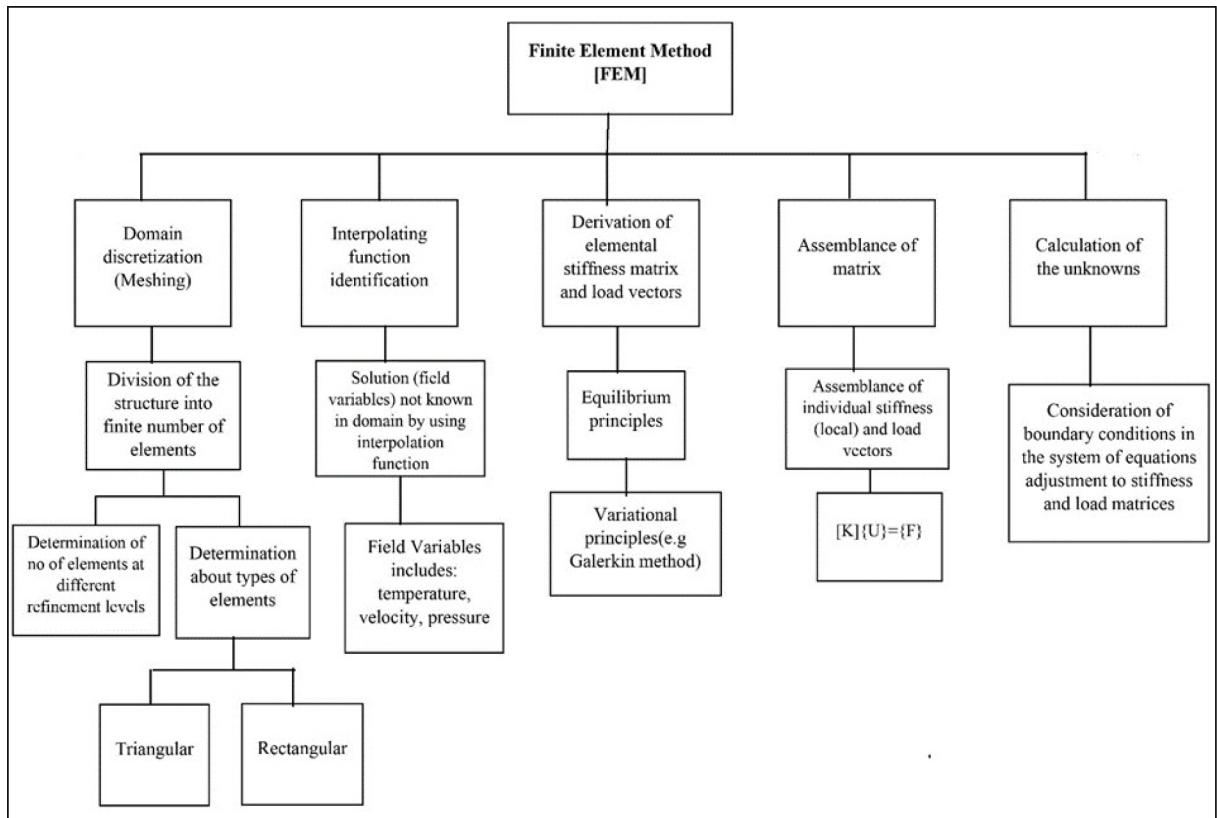


Fig. 3. Diagram representing steps involved in scheme.

$$\int_{\Omega} \left(U^* \frac{\partial V^*}{\partial X^*} + V^* \frac{\partial U^*}{\partial Y^*} \right) w d\Omega + \int_{\Omega} \frac{\partial P^*}{\partial Y^*} w d\Omega + Pr \int_{\Omega} \left[\left(1 + \frac{1}{\beta} \right) \left(\frac{\partial V^*}{\partial X^*} + \frac{\partial V^*}{\partial Y^*} \right) + \Lambda_{y^*} \right] w d\Omega = 0 \quad (28)$$

$$U^* \approx U_h^* \in W_h, V^* \approx V_h^* \in W_h, \theta^* \approx \theta_h^* \in W_h, C^* \approx C_h^* \in W_h, P^* \approx P_h^* \in Q_h \quad (32)$$

$$\int_{\Omega} \left(U_h^* \frac{\partial U_h^*}{\partial X^*} + v \frac{\partial U_h^*}{\partial Y^*} \right) w_h d\Omega + \int_{\Omega} \frac{\partial P_h^*}{\partial X^*} w_h d\Omega - Pr \int_{\Omega} \left(1 + \frac{1}{\beta} \right) \left(\frac{\partial^2 U_h^*}{\partial X^{*2}} + \frac{\partial^2 U_h^*}{\partial Y^{*2}} \right) w_h d\Omega + \Lambda_{X^*} = 0 \quad (33)$$

$$\int_{\Omega} \left(U_h^* \frac{\partial V_h^*}{\partial X^*} + V_h^* \frac{\partial V_h^*}{\partial Y^*} \right) w_h d\Omega + \int_{\Omega} \frac{\partial P_h^*}{\partial X^*} w_h d\Omega - Pr \int_{\Omega} \left(1 + \frac{1}{\beta} \right) \left(\frac{\partial^2 U_h^*}{\partial X^{*2}} + \frac{\partial^2 U_h^*}{\partial Y^{*2}} \right) w_h d\Omega + \Lambda_{Y^*} = 0 \quad (34)$$

Integral form of mass conservation equation is described as under.

$$\int_{\Omega} \left(\frac{\partial U^*}{\partial X^*} + \frac{\partial V^*}{\partial Y^*} \right) q d\Omega = 0 \quad (29)$$

$$\int_{\Omega} \left(U^* \frac{\partial \theta^*}{\partial X^*} + V^* \frac{\partial \theta^*}{\partial Y^*} \right) w d\Omega - \int_{\Omega} \left(\frac{\partial^2 \theta^*}{\partial X^{*2}} + \frac{\partial^2 \theta^*}{\partial Y^{*2}} \right) w d\Omega = 0, \quad (30)$$

$$\int_{\Omega} \left(U^* \frac{\partial C^*}{\partial X^*} + V^* \frac{\partial C^*}{\partial Y^*} \right) w d\Omega - \frac{1}{Le} \int_{\Omega} \left(\frac{\partial^2 C^*}{\partial X^{*2}} + \frac{\partial^2 C^*}{\partial Y^{*2}} \right) w d\Omega = 0$$

Continuous solutions is approximated by discrete ones in the finite dimensional sub-spaces.

$$\int_{\Omega} \left(\frac{\partial U_h^*}{\partial X^*} + \frac{\partial V_h^*}{\partial Y^*} \right) q d\Omega = 0, \quad (35)$$

$$\int_{\Omega} \left(U_h^* \frac{\partial \theta_h^*}{\partial X^*} + V_h^* \frac{\partial \theta_h^*}{\partial Y^*} \right) w_h d\Omega - \int_{\Omega} \left(\frac{\partial^2 \theta_h^*}{\partial X^{*2}} + \frac{\partial^2 \theta_h^*}{\partial Y^{*2}} \right) w_h d\Omega = 0, \quad (36)$$

$$\int_{\Omega} \left(U_h^* \frac{\partial C_h^*}{\partial X^*} + V_h^* \frac{\partial C_h^*}{\partial Y^*} \right) w_h d\Omega - \int_{\Omega} \left(\frac{\partial^2 C_h^*}{\partial X^{*2}} + \frac{\partial^2 C_h^*}{\partial Y^{*2}} \right) w_h d\Omega = 0, \quad (37)$$

In matrix representation.

Table 2

Mesh independence for mean heat and mass fluxes.

Grid	Nu_{avg}	Sh_{avg}	K.E.
Extremely coarse	7.6644	1.6335	545.91
Extra coarse	7.7575	1.5015	552.88
Coarser	7.8530	1.3531	558.65
Coarse	8.1099	1.1601	551.95
Normal	8.2137	1.1145	549.11
Fine	8.3375	1.0528	547.71
Finer	8.6075	0.97155	545.58
Extra fine	8.7525	0.94589	543.65
Extremely fine	8.7504	0.94173	543.67

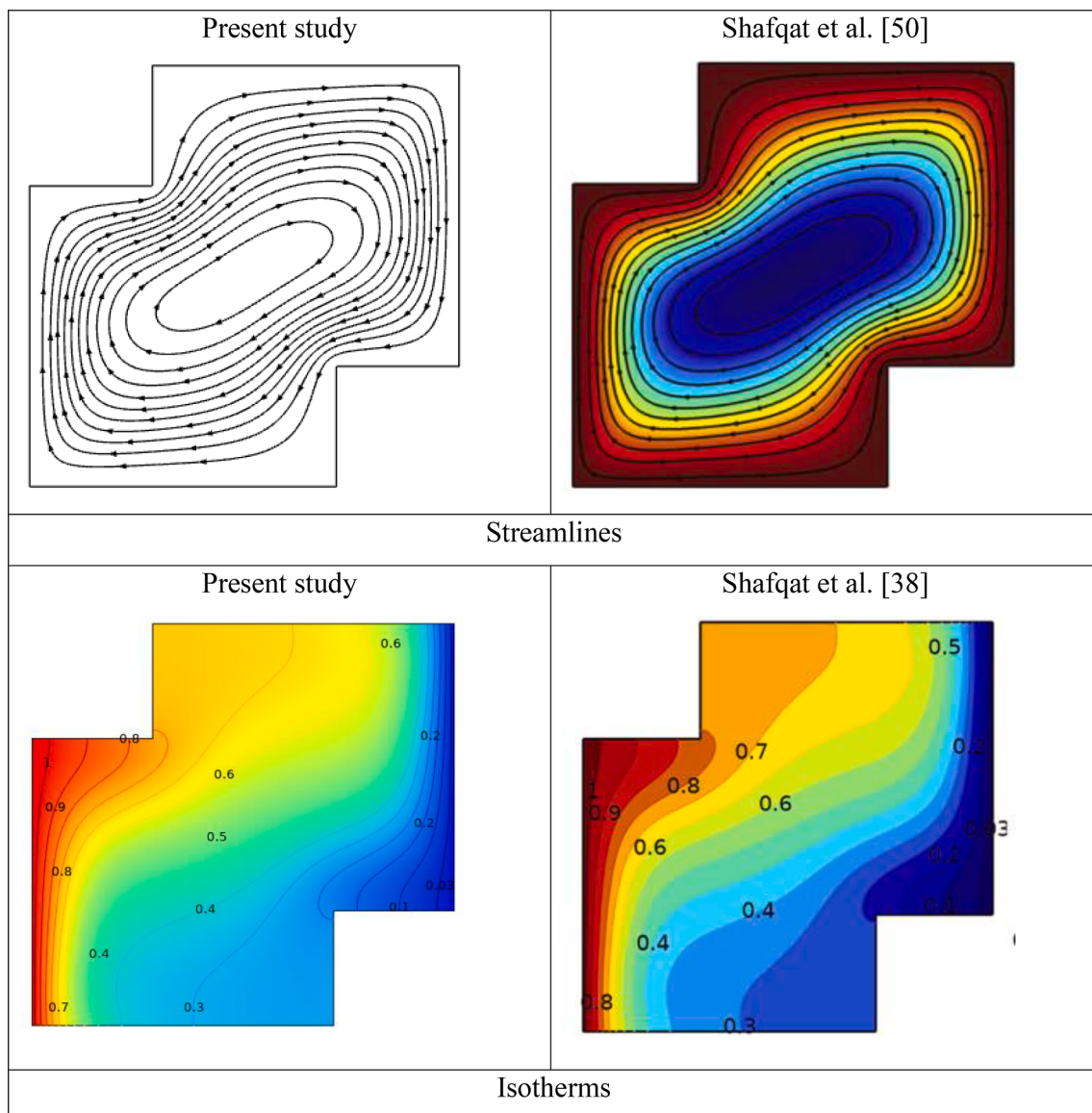
Table 3Conformity of results for Nusselt number against different value of β .

β	Shafqat et al. [48]	Present
0.1	2.38986	2.39023
1	3.81194	3.81168
5	4.27587	4.27511
10	4.35556	4.35470

$$\begin{bmatrix}
 Pr.L_h + N(U_h^*, V_h^*) & 0 & B_1 & 0 \\
 0 & Pr.L_h + N_h(U_h^*, V_h^*) & B_2 & -RaPrM_h \\
 B_1^T & B_2^T & 0 & 0 \\
 0 & 0 & 0 & L_h + N_h(U_h^*, V_h^*)
 \end{bmatrix}
 \begin{bmatrix}
 U^* \\
 V^* \\
 P^* \\
 \theta^*
 \end{bmatrix}
 =
 \begin{bmatrix}
 F_1 \\
 F_2 \\
 F_3 \\
 F_4 \\
 F_5
 \end{bmatrix}
 \quad (38)$$

which can be written as: $A\xi = F$

L_h : Discrete Laplace matrix, N_h : Non-linear convection matrix, M_h : Mass matrix, ξ : Solution vector, F : Right hand side after implementation of boundary condition. To compute the solution, this non-linear system is iterated till a specified convergence criterion is met. The

**Fig. 4.** Stream lines and isothermal contours presentation to depict agreement of results.

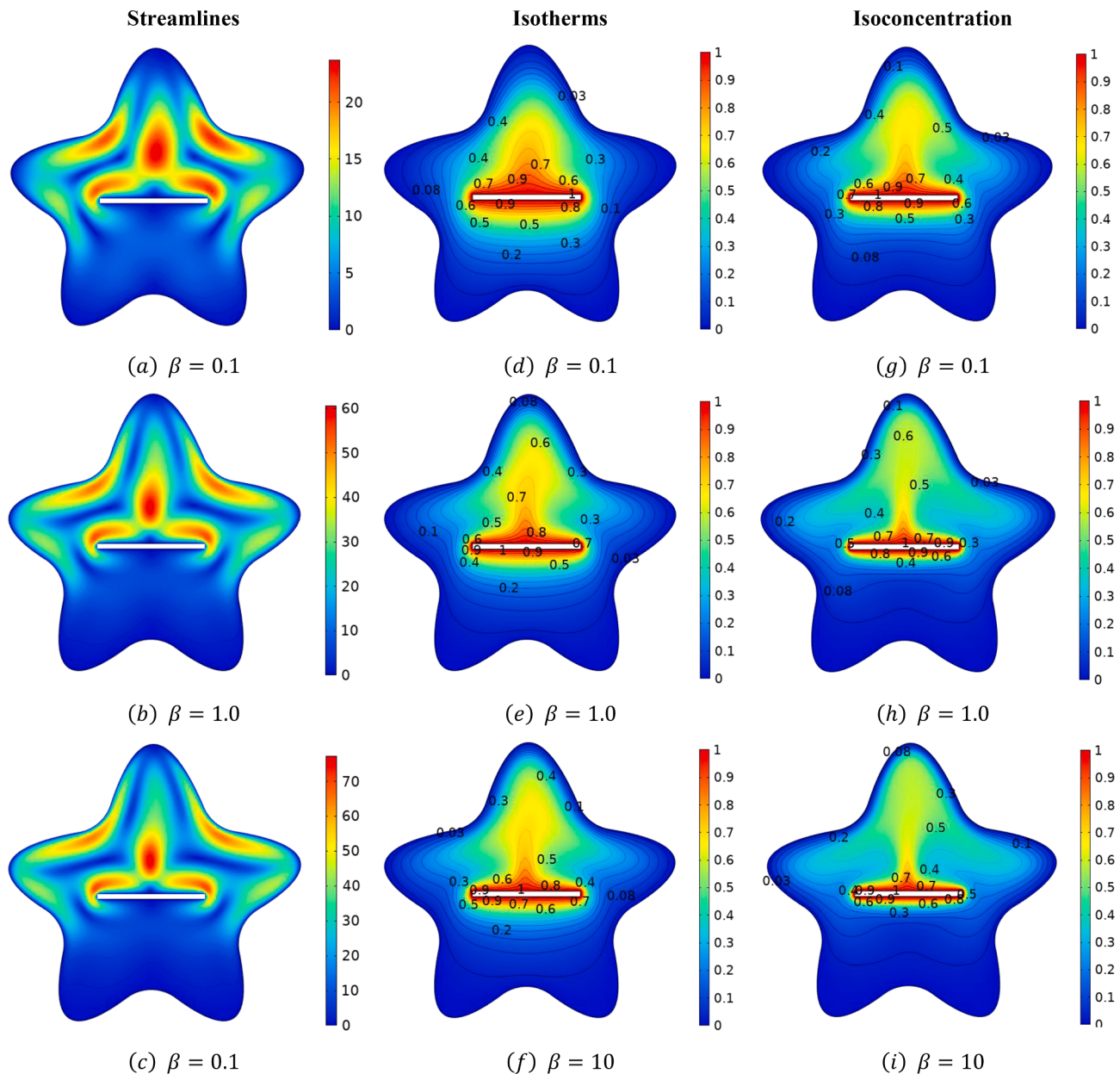


Fig. 5. Variation in velocity, thermal and solutal concentrated fields against (β).

nonlinear iterations are stopped when the residual is dropped by 10^{-6} .

Mesh independence test

Efficiency of implemented numerical scheme is checked in Table 2 by performing mesh independence test by changing refinement levels and by fixing all involved physical parameters. Estimation about global quantities like Kinetic energy, Nusselt and Sherwood numbers are measured and found complete match between level 8 and 9.

Results validation

Credibility of presently computed finding is assured by making match with results presented by Shafqat et al. [48] as shown in Table 3. Here, heat flux coefficient is measured against Casson parameter and strong agreement between available and current studies is found. This agreement of results is graphically visualized in Fig. 4.

Results and discussion

This portion is presented to adumbrate the impression of involved physical parameters on associated distribution via streamlines, contour plots for temperature and species deposition. Initially, system of governing equations are modelled in the form of PDEs and solved by implementing finite element approach. To enrich attraction in current work for engineers some valuable globally and locally distributed quantities like kinetic energy, Nusselt number and Sherwood numbers are also measured.

Change in velocity, thermal and solutal profiles versus wide range of Casson parameter (β) is elaborated in Fig. 5. Description about deviation in flow of non-Newtonian fluid against (β) is divulged in Fig. 5(a-c). Since by increasing (β) the flow behavior of considered non-Newtonian approaches towards Newtonian fluid so velocity field is found to decreasing function of (β). Thus, at lower magnitude of (β) stream patterns are more than in case of $\beta = 10$. Response of temperature distribution against (β) is manifested in Fig. 5(d-f). It is seen that positive

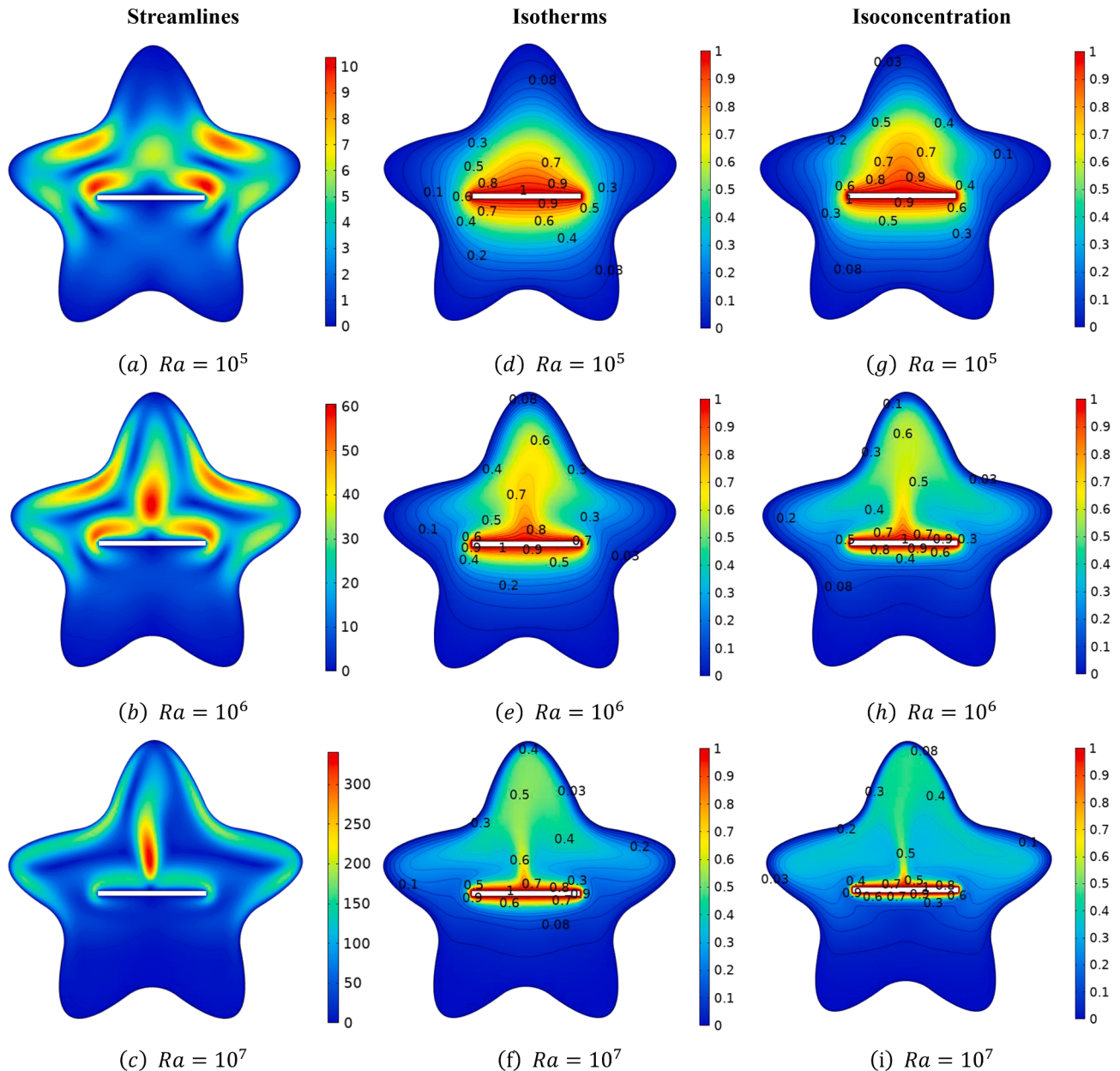


Fig. 6. Variation in velocity, temperature and solutal concentrated fields against Rayleigh number (Ra).

trend in magnitude of temperature is observed at $\beta = 10$ because velocity at this magnitude of (β) is high than at $\beta = 0.1$. So, the average kinetic energy is also higher which describes the temperature distribution. Influence of Casson parameter (β) on species mass distribution is interpreted in Fig. 5(g-i). At lower values of (β) dominance in accumulation of particles is attained because viscosity of fluid is more rather than in case of $\beta = 10$. Additionally, due to provision of constant mass distribution at rectangular plate more solutal convective potential is generated in upper region of enclosure.

Wide range of Rayleigh number (Ra) is opted to discuss its effectiveness on velocity, temperature and concentration field as shown in Fig. 6(a-i). Positive trend in magnitude of stream function assigned for comprehension of velocity field is evaluated against (Ra) in Fig. 6(a-c). It is because of the fact that (Ra) has direct relation with temperature gradient between cold and hot portions in domain and has inverse relation with viscosity. So, by uplifting (Ra) viscosity of fluid decreases and momentum diffusivity of particles enriches. Description about effectiveness of (Ra) on thermal profile is discussed in Fig. 6(d-f).

Enhancement in temperature of fluid is attained due to generation of extensive temperature difference between cold and hot regions of enclosure. Due to this fact thermal convective potential is generated which mounts the role of thermal buoyancy force and thus as an outcome temperature of fluid upsurges. Response of solutal concentration versus (Ra) is measured in Fig. 6(g-i). It is revealed that concentration of fluid is extensive for high values of (Ra). This is justified by the fact that at lower magnitude of (Ra) fluid accumulates more due to production of minute concentration differences and contrary to it the concentration field exceeds.

Role of magnetic field parameter (Ha) on momentum, thermal and solutal concentrated profiles are examined in Fig. 7(a-i). Since the appliance of magnetization to the flow generates resistive force to the fluid which causes reduction in velocity field and produces laminar field. So, it is found in Fig. 7(a-c) that at higher magnitude i.e. $Ha = 60$ lower magnitude of velocity is attained. Similarly, decrementing trend in temperature distribution delineated from isothermal contours is determined in Fig. 7(d-f). It is due to the reason that by incrementing (Ha)

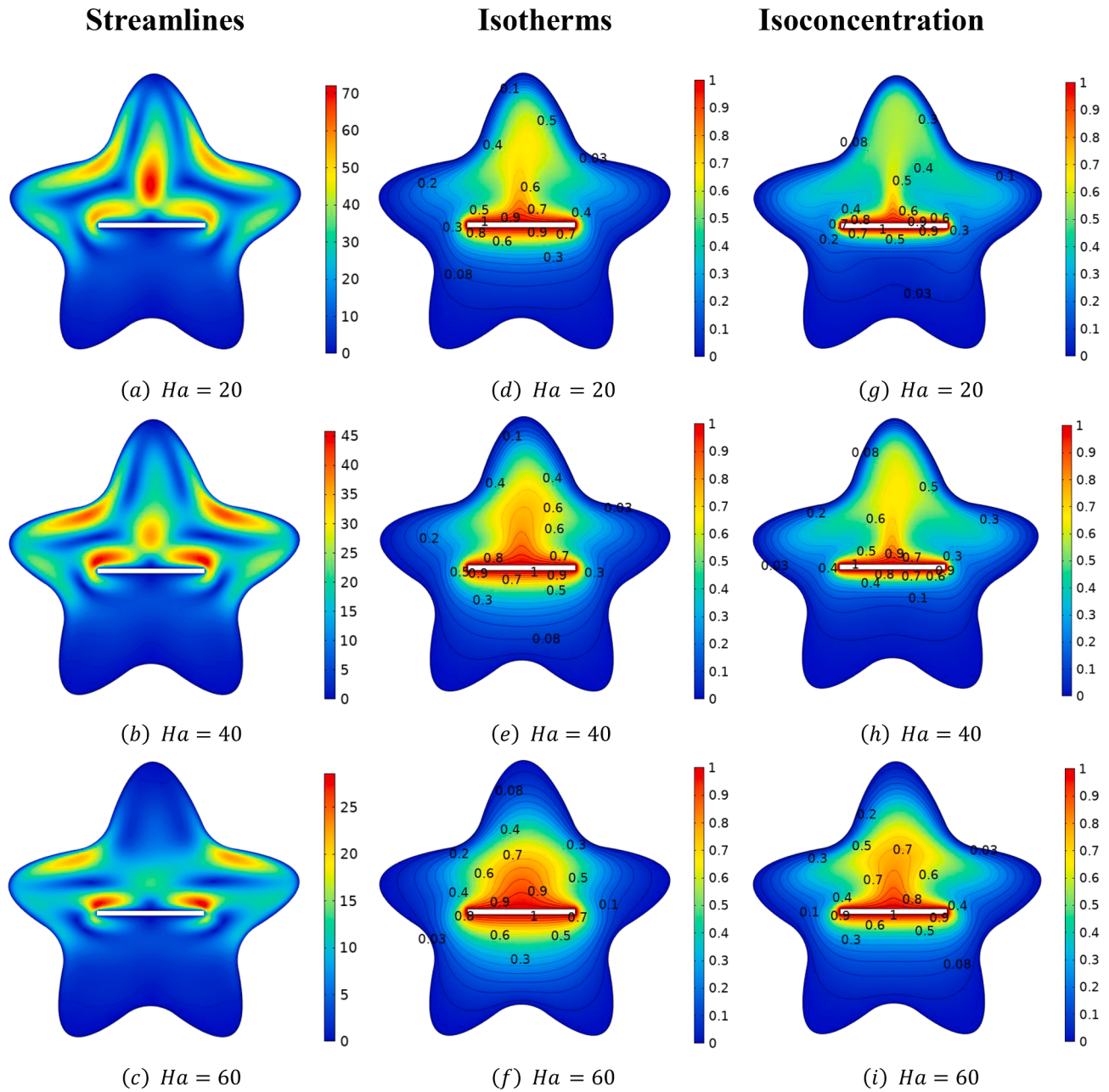


Fig. 7. Variation in velocity, thermal and solutal concentrated fields against Hartmann number (Ha).

average kinetic energy of particles decreases which as an outcome diminishes the temperature of fluid. Since, viscosity of fluid shows increasing trend against (Ha) due to production of Lorentz resistive force so the particles accumulate and concentration field mount which is evidenced in Fig. 7(g-i).

Exploration about implication of Lewis number (Le) on velocity, thermal and solutal concentrated fields is manifested in Fig. 8(a-i). No significant changes in velocity and temperature fields are found against (Le) in Fig. 8(a-f) because no direct correspondence with momentum and thermal diffusivities exist. Whereas, in view of concentration distribution it depreciates against increasing values of Lewis number (Le) as shown in Fig. 8(g-h). In addition, solutal boundary layer near the rectangular plate where constant concentration distribution is capitalized becomes thinner at $Le = 10$.

Table 4 enumerates numerical data examining variation in (Nu_{avg}) and (Sh_{avg}) against (Ha) and (β). At $Ha = 0$ maximum magnitude of heat flux coefficient is attained whereas lowest values of mass flux is attained

and contrary aspects are attained at $Ha = 100$ for both physical quantities. This is justified by the fact that at $Ha = 0$ no magnetic field is present which allows the particles to move freely in the domain due to which average kinetic energy enhances and associated heat flux rate uplifts whereas the concentration of fluid particles does not accumulate.

Description about deviation in kinetic energy for wide range of Hartmann number (Ha) and Casson parameter (β) is explicated in Table 5. It is found that kinetic energy at $\beta = 10$ and in the absence of magnetic field is increased by 17.5 times more than for $\beta = 0.1$. The reason behind this phenomenon is that the Casson fluid approaches towards Newtonian case for higher magnitude and viscosity of fluid becomes constant. So, the kinetic energy of particles raises and additionally no magnetic field is present in this case so no resistive forces are generated.

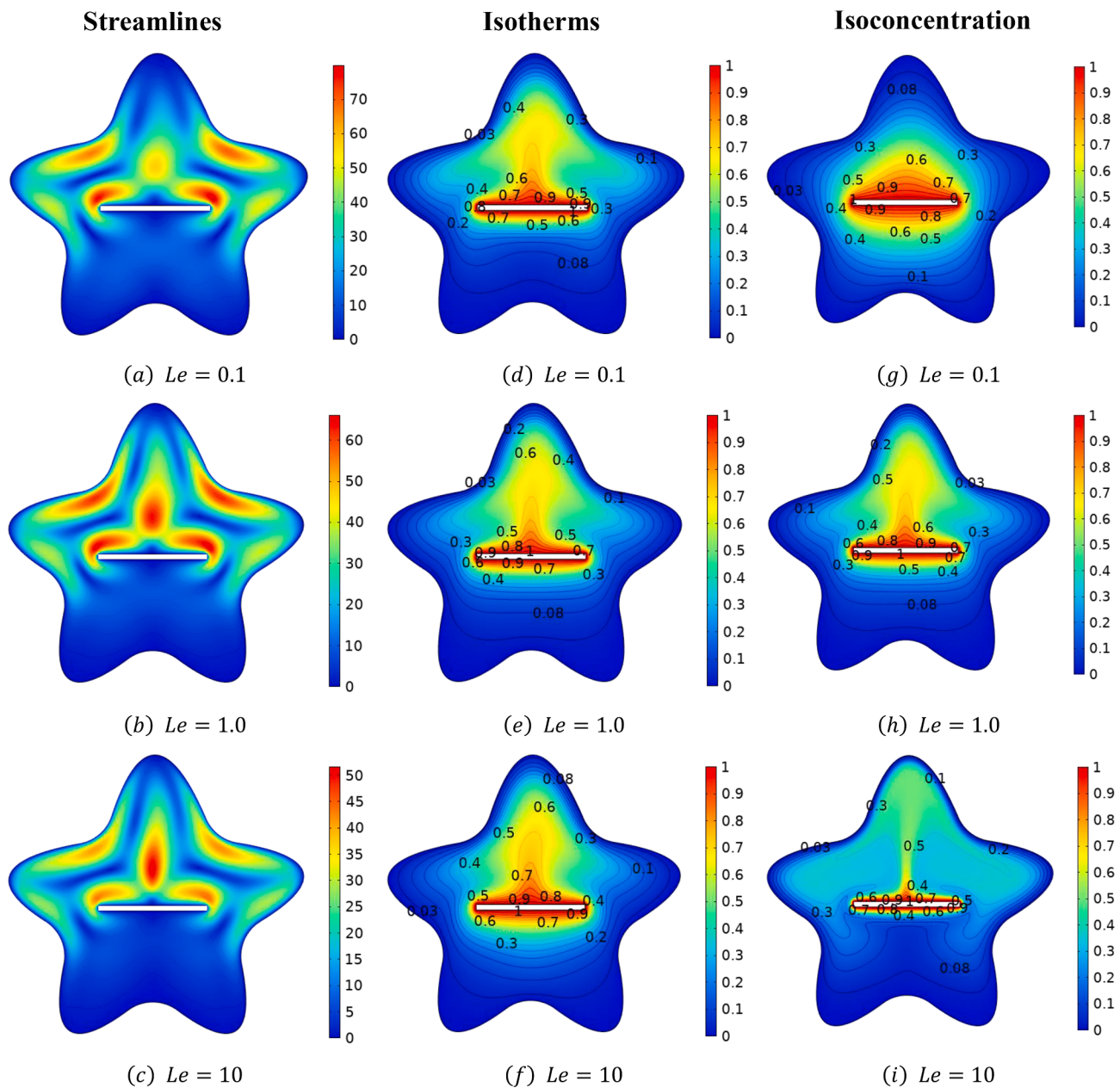


Fig. 8. Variation in velocity, thermal and solutally concentrated fields against Lewis number (Le).

Table 4

Variation in average Nusselt and Sherwood numbers against (β) and (Ha).

Nu_{avg}				Sh_{avg}		
Ha	$\beta = 0.1$	$\beta = 1$	$\beta = 10$	$\beta = 0.1$	$\beta = 1$	$\beta = 10$
0	5.5438	8.6040	9.8667	0.50247	0.69399	1.86590
25	5.3113	7.6715	8.6307	0.51889	0.94431	1.1848
50	4.8982	6.3915	6.9751	0.50954	0.78901	0.99334
75	4.5724	5.4352	5.7578	0.50348	0.47608	0.56004
100	4.3699	4.8232	4.9835	0.54370	0.39405	0.41644

Conclusion

The prime objective of this work is to adumbrate characteristics of thermal and solutal convection in Casson fluid enclosed in star cavity with corrugations. Additionally, rectangular plate of unit length is adjusted in the domain and uniform thermal and solutal distributions

Table 5

Variation in kinetic energy against (β) and (Ha).

K. E			
Ha	$\beta = 0.1$	$\beta = 1$	$\beta = 10$
0	148.31	1370.6	2534.6
25	107.34	543.65	765.81
50	55.878	168.55	204.11
75	27.729	63.363	72.620
100	13.934	26.755	29.750

are provided. Formulation of problem is conceded in the form of dimensionless equations and solve numerically by finite element based commercial software (COMSOL). Some salient key findings are enlisted below.

- i) Decrementing trend in velocity is observed against Hartmann number (Ha) due to generation of resistive forces in the domain.
- ii) At lower values of Casson parameter (β) velocity as well as kinetic energy exhibits decreasing aspects.
- iii) Rayleigh number (Ra) causes uplift in temperature distribution whereas the concentration profile depicts.
- iv) Lewis number (Le) has inverse relation with mass diffusivity and no prominent effect on velocity and temperature fields.
- v) Intensification in kinetic energy is revealed against (Ha) whereas contrary attribute is observed against (β).
- vi) Heat and mass flux coefficients show diminishing aspects against Hartmann number (Ha).
- vii) Heat and mass flux distribution exhibit upsurging behaviour against Casson parameter (β).

CRediT authorship contribution statement

Imtiaz Ali Shah: Conceptualization, Writing – original draft. **S. Bilal:** Methodology. **Arshad Riaz:** Writing – review & editing, Investigation. **ElSayed M. Tag El-Din:** Funding acquisition, Software. **M.M. Alqarni:** Validation. **Haneen Hamam:** Validation, Methodology.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Data availability

Data will be made available on request.

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